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Electrically Heated Wire Catalyst for Cold Start Emission

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Three way catalysts were dispersed over the surface of an anodized Ti wire in order to promptly eliminat hydrocarbons remained in cold-start-exhaust gas from an automobile engine. The anodized wire was heated u to 623K or higher up to 30 sec simply by loading 13V to the ends of wire, which resulted in abatement of 50% hydrocarbons in the cold-start-exhausts within 30 sec just after engine ignition.

Three-way catalysts, usually equipped for gasoline engine automobiles, work well at the temperatures higher than 623K and are heated up to this temperature in a few minutes by an exhaust gas itself. Thus, the pollutants in the exhaust gases in a first few minutes after an engine ignition (cold-start-exhausts) are not well eliminated, since the catalysts are not sufficiently heated.¹⁾ Hydrocarbons, not burned in an engine room, are the main pollutant in the cold-start-exhausts, and more than 20% of the unburned hydrocarbons are $C_2 \sim C_4$ olefins which will cause the destruction of ozone layer.²⁾

The purpose of this work is to develop a catalyst system devised for the abatement of unburned hydrocarbons remained in the cold-start-exhausts. The paper consists of two parts in the firs part the preparation and characterization of anodized Ti wire catalysts will be mentioned, and in the second part an application of the wire catalysts to cold-startexhausts including NO, propene, oxygen and water vapor will be discussed.

A spiral Ti wire (1m x 0.25 mm od, 99.6% purity) was anodized at 80V for 30min in a 0.16M oxalic

electrolyte at 303K using a graphite cathode and regulator dc supply.³⁾ The current observed wa rapidly depressed in the first 10 sec of anodizing an then gradually decreased to a constant value (3 mA). The first depress in the current through a 7 wire means the formation of titanium oxide films



Fig.1 SEM photograph of anodic oxide films formed on Ti wire

over the Ti wire surface. Judging from SEJ photograph, given in Figure 1, of the oxide film calcined at 873K for 4h, the oxide films are about μ thick and less porous.

X-ray crystallographic structure of the titanium

oxide films formed over the wire surface was deduced by measuring X-ray diffraction spectra of the oxide films formed on a Ti thin plate, which was anodized under the same conditions employed for the wire. X-ray spectrometer was operated at 30 kV and 15 mA using a Ni filter for CuK α radiation. X-ray diffraction patterns of the oxide films formed on Ti thin plates calcined at 673, 873, and 1023K are shown in Figure 2. Although no diffraction peaks assigned to rutile were observed for the sample calcined at 1023K. While for the oxide films calcined at 1023K, peaks attributed to anatase and rutile were detected because of the anatase transformation of crystal structure at 893K.⁴⁾ Two



Fig.2 X-ray diffraction pattern of anodic oxide films calcined at (a)673K, (b)873K, and (c)1023K, respectively.

peaks marked by a solid triangle in the Figure could be assigned to Ti_2O_3 by comparison with the pattern given in files for X-ray powder diffraction.⁵⁾ Consequently, crystallographic structure of the oxide films formed over the Ti wire determined to be the mixture of anatase, rutile, and Ti_2O_3 when the anodized wire was calcined at 873K.

The anodized wires calcined at 873K were immersed with a suspension of fibrillar boehmite sols, prepared by hydrolysis of aluminum isopropoxide,⁵⁾ mixed with aqueous solutions of palladium, rhodium, and cerium nitrates, although



Fig.3 Wire catalysts inserted into each cell of a ceramic honeycomb.

palladium nitrate was hard to be dissolved into water. The immersed wires dried and calcined at 873K for 4h again, followed by inserting into each cell of a ceramic honeycomb, as shown in Figure 3. Amounts of Pd, Rh, and CeO₂ loaded on Al₂O₃ were 0.2, 0.7 and 25.0wt%, respectively, measured by X-ray fluorescent spectroscopy, and about 0.2 mg of the catalyst was dispersed on the surface of an anodized wire. The ends of wires were connected with each Cu electrode equipped with a quartz reactor. The wires were promptly heated by charging a voltage to the ends of wire in flowing He, and the wire temperature were estimated by monitoring the currents passing through wires.⁶⁾ As given in Figure 4, the temperature rapidly reached to the constant values in 30 sec after charging.

The quartz reactor including the wire catalysts was settled in a flow system, which supplies the gases



Fig.4 Variation of surface temperature after charging a voltage to the ends of wire.

consisting of C₃H₆(1000ppm), NO(1000ppm), O₂ (1%) and water vapor(15%), diluted by He, into the reactor with a flow rate of 10L/hr. At the outlet of the reactor, the concentrations of C_3H_6 and NO were measured by mass spectrometer and NOx analyzer. In Figure 5 are given the results obtained when 13V was charged to the ends of wire catalysts. In the first stage of the reaction, a part of C_3H_6 were burned by the reaction, a part of C_3H_6 were burned by reaction with O_2 and then with NO, suggesting the difference in the light off temperatures between the reactions of C_3H_6/O_2 and C_3H_6/NO . It was found that more than 50% of C_3H_6 were burned out by charging 13V for 30 sec, and around 70% for successive 30 sec charging. By charging 13V for 150 sec, the conversion of C_3H_6 reached to 90% or more, hence the removal of NO began to decrease. This is the same when one will plot the conversion of both C_3H_6 and NO against the reaction temperature, instead of the charging time, for the three-way powder catalyst. It should be noted that the conversion curve of C_3H_6 in the Figure was well reproduced in the absence of NO, suggesting that the reaction of C_3H_6/O_2 proceeded well without the acid by NO and NO₂.

One of the problems for electrically heated catalyst (EHC) systems is how much electricity is needed for the abatement of pollutants in automobile exhausts, since the capacity of battery equipped is usually limited to 12 or 24V. In the present work, the current passing through wire catalysts is 21A with a load of 13V, then the electricity required will be around 273W, which seems to be adequately small for practical use.



Fig.5 Rapid removal of C_3H_6 and NO by wire catalysts charged by 13V in the presence of O_2 and water vapor.

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